



# Model-based description of droplet deformation into polyhedral shapes in liquid-liquid polydisperse dense-packed zones

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## ABSTRACT

Droplet deformation in liquid-liquid dense-packed zones (DPZs) significantly impacts the dispersed phase volume fraction and droplet coalescence, which is crucial to phase separation processes in various industrial equipment. This study introduces a modeling approach to describe droplet deformation into polyhedral shapes in polydisperse DPZs. Droplet deformation, characterized by the contact radius  $r_f$ , the curvature radius  $r_a$ , and the volume ratio  $\epsilon_i$  is modeled using equations based on pressure, geometric, and volumetric relationships for regular polyhedra as well as Bond number correlations. Moreover, generalized Bond number correlations are proposed to extend the approach to irregular convex polyhedral shapes. Simulations across technical Bond number ranges demonstrate that  $r_f$  and  $\epsilon_i$  increases with the Bond number, while  $r_a$  decreases, approaching zero at high Bond numbers. The Bond number correlations strongly agree with equation-based solutions, with mean absolute percentage errors below 3.0 %. Practical implications include enhanced predictions for DPZ behavior and integration into a common coalescence model.

## 1. Introduction

The deformation of droplets in liquid-liquid dense-packed zones (DPZ) affects the volume fraction of the dispersed phase within the DPZ (Henschke, 1995; Lacasse et al., 1996; Abe and Inasawa, 2022; Sibirtsev et al., 2025) as well as the droplet coalescence (Henschke, 1995, 2002; Chan et al., 2011; Bozzano and Dente, 2010). Both the dispersed phase volume fraction and droplet coalescence significantly impact the formation and dissolution of the DPZ, thereby influencing the phase separation behavior of liquid-liquid dispersions (Henschke, 1995, 2002; Thaker and Buwa, 2019; Steinhoff et al., 2018).

Since DPZs are encountered in various types of equipment used for liquid-liquid phase separation processes - such as batch-settling cells (Henschke, 1995; Sibirtsev et al., 2024; Leleu and Pfennig, 2019; Sibirtsev et al., 2019), stirred and sieve tray columns (Weber and Jupke, 2020; Sovilj et al., 2019; Graham et al., 1979; Mohanty and Vogelpohl, 1997), vertical and horizontal gravity settlers (Rommel et al., 1992; Frising et al., 2006; Schlieper et al., 2004; Ye et al., 2023b; Steinhoff et al., 2021), batch stirred tanks (Ye et al., 2023a), and centrifugal extractors (Eggert et al., 2019) - an accurate, model-based description of droplet deformation, and consequently the DPZ, is essential for the proper design of such equipment.

Henschke (1995) developed a model to describe droplet deformation within the DPZ, which has been successfully applied to batch-settling

cells (Henschke, 2002; Leleu and Pfennig, 2019; Eberz et al., 2025), horizontal gravity settlers (Henschke, 1995; Schlieper et al., 2004), and batch stirred tanks (Ye et al., 2023a). However, this model assumes that the DPZ is formed by a monodisperse droplet size distribution (Henschke, 1995). This assumption limits the level of detail in the deformation modeling, potentially leading to an underestimation of the DPZ height (Henschke, 1995), and thus, an increased risk of apparatus flooding.

In technical applications, the DPZ is typically formed by a polydisperse droplet size distribution (Thaker and Buwa, 2019; Thaker et al., 2018; Raynel et al., 2023). Therefore, improving the accuracy of DPZ height predictions requires increasing the level of detail in deformation modeling by accounting for polydispersity.

This study introduces a modeling approach for droplet deformation into polyhedral shapes, accounting for the polydispersity of the DPZ. The approach is based on pressure, geometrical, and volumetric relationships generally applicable to regular polyhedral shapes: tetrahedron, cube, octahedron, dodecahedron, and icosahedron. These polyhedral shapes are characteristic for random loose packings of polydisperse, deformed droplets (Sibirtsev et al., 2025). Furthermore, generalized semi-empirical correlations based on the Bond number ( $Bo$ ) are proposed to describe the deformation of droplets into both regular and irregular convex polyhedral shapes.

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Nomenclature			
$a$	Edge length of the polyhedron	$p_{f,min}$	Minimum pressure acting on the contact area between droplets
$a_0$	Initial guess for the edge length	$p_h$	Hydrostatic pressure
$a_{max}$	Maximum edge length	$p_{in}$	Pressure inside the droplet
$a_{min}$	Minimum edge length	$p_{out}$	Pressure outside the droplet
$A_j$	Value of the iterative solution	$p_{out,c}$	Pressure outside the droplet in the center of the drainage film
$A_a$	Area of the circular segment	$p_{out,r}$	Pressure outside the droplet behind the rim
$A_c$	Channel area	$p_s$	Excess pressure within the drainage film
$A_f$	Contact area between droplets	$P_j$	Predicted values by the Bond number correlation
$A_p$	Polyhedral face area	$P$	Intersecting point
$A_s$	Intersection area	$p$	Pressure
$A_t$	Area of an isosceles triangle	$r_a$	Radius of droplet's curvature regions
$Bo$	Bond number	$r_{a,0}$	Initial guess for the curvature radius
$b$	Polyhedron edge	$r_{a,max}$	Maximum curvature radius
$C_A$	Polyhedral shape constant	$r_{a,min}$	Minimum curvature radius
$C_{cor}$	Correction factor	$r_c$	Incircle radius of the polygon representing the polyhedron's face
$C_{rc}$	Polyhedral shape constant	$r_{eq}$	Equivalent droplet radius
$C_{rm}$	Polyhedral shape constant	$r_f$	Radius of the contact areas between droplets
$C_{rs}$	Polyhedral shape constant	$r_{f,0}$	Initial guess for the contact area radius
$C_V$	Polyhedral shape constant	$r_{f,max}$	Maximum contact area radius
$C_j$	Fitting parameter	$r_{f,min}$	Minimum contact area radius
$E_{L,j}$	Results of the left hand side equation	$r_o$	Incircle radius of contact area's polygon
$E_{R,j}$	Results of the right hand side equation	$r_s$	Polyhedron's insphere radius
$h_{eq}$	Equivalent DPZ height	$V_c$	Channel volume
$h_i$	Height of the DPZ acting on the droplet	$V_p$	Polyhedron volume
$MAPE_j$	Mean absolute percentage error	$V$	Droplet's volume
$N_c$	Number of polyhedron corners	$x$	Distance between point $P$ and the polygon border
$N_E$	Number of equations	$y$	Polyhedron edge length
$N_e$	Number of polyhedron edges	$\alpha$	Half the angle between two polyhedron faces
$N_{fc}$	Number of polyhedron's face corners	$\bar{\epsilon}_p$	Average volume fraction of the dispersed phase in the DPZ
$N_p$	Number of fitted points	$\epsilon_{i,max}$	Maximum volume fraction
$N_r$	Number of calculation results	$\epsilon_{i,min}$	Minimum volume fraction
$p_i$	Pressure acting on the droplet $i$	$\epsilon_i$	Volume fraction
$p_d$	Excess pressure inside the droplet	$\delta$	Triangle angle
$p_{eq}$	Equivalent pressure	$\Delta\rho$	Density difference between the two liquid phases
$p_f$	Pressure acting on the contact area between droplets	$\sigma$	Interfacial tension
$\bar{p}_f$	Pressure at all deformation stages	$\Psi$	Substitution
$p_{f,max}$	Maximum pressure acting on the contact area between droplets		

## 2. Fundamentals

The degree of droplet deformation within a DPZ is governed by the interplay between the buoyancy force exerted by the DPZ and the deformation resistance of the droplets, which is determined by interfacial tension (Henschke, 1995). Deformation leads to the formation of plane contact areas between droplets and regions of curvature, ultimately shaping the droplets into polyhedral structures (Lacasse et al., 1996; Abe and Inasawa, 2022; Thaker and Buwa, 2019; Höhler and Weaire, 2019). While the exact deformation shape can be predicted using Morse-Witten theory (Morse and Witten, 1993), this method is computationally intensive (Höhler and Weaire, 2019; Dunne et al., 2019).

However, knowledge of the exact deformation shape is not required to determine the volume fraction of the dispersed phase or droplet coalescence within the DPZ, which is critical for the formation and dissolution of the DPZ. To address this, Henschke (1995) proposed a less computationally intensive model that assumes a monodisperse droplet size distribution forms the DPZ and that the droplets deform into a dodecahedron shape. The model is based on an equation system involving pressure, geometrical, and volumetric relationships and is solved iteratively. In Henschke's model, droplet deformation is characterized by

two radii:  $r_f$ , which represents the radius of the contact areas between droplets, and  $r_a$ , which describes the radius of droplet's curvature regions. Moreover, the edge length  $a$  of the polyhedron is a required parameter to determine  $r_f$  and  $r_a$ .

In addition to the equation system, Henschke introduced semi-empirical  $Bo$  number correlations. During deformation, the gravitational and interfacial tension forces act on the droplet's interface. While the gravitational force favors deformation, the interfacial tension force counteracts deformation. The resulting equilibrium of forces determines the degree of deformation. The  $Bo$  number represents the ratio of gravitational force to interfacial tension force and, thus, is suitable for a model-based description of droplet deformation. The  $Bo$  number correlations are fitted to the results of the iterative solution of the equation system and, while less computationally intensive, effectively captures the dependence of  $r_f$ ,  $r_a$  on the relevant influencing parameters (Henschke, 1995). Furthermore, Henschke proposed a model for calculating droplet coalescence within the DPZ based on  $r_f$  and  $r_a$  (Henschke, 1995, 2002).

However, the derivation of the deformation model (Henschke, 1995) is partially challenging to interpret and limited to the dodecahedron shape. Moreover, the source of the derivation is written in German,

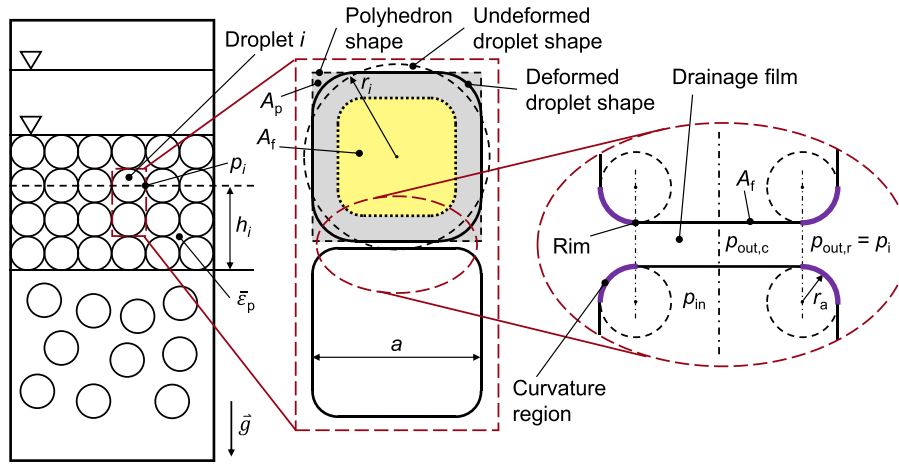


Fig. 1. Relevant parameters during the droplet deformation of two equal-sized droplets into a cubic shape.

which makes it less internationally accessible. A later publication (Henschke, 2002), written in English, aimed to present the model but introduced equations that conflict with the original source (Henschke, 1995) and are mathematically inappropriate for describing certain relationships. For example, the equation proposed for the asymptotically decreasing curve of  $r_a$  (Henschke, 2002) fails to accurately reflect the mathematical behavior described in the original work (Henschke, 1995).

In technical applications, the DPZ is typically formed by a polydisperse droplet size distribution (Thaker and Buwa, 2019; Thaker et al., 2018; Raynel et al., 2023). This polydispersity leads to the formation of various polyhedral shapes during droplet deformation. The deformation shape in a polydisperse DPZ is influenced by the droplet's contact number, representing the number of neighboring droplets in contact with a given droplet (Sibirtsev et al., 2025; Liu et al., 2019).

Sibirtsev et al. conducted a model-based study on droplet contact numbers in liquid-liquid DPZs formed by log-normal and Gaussian droplet size distributions (Sibirtsev et al., 2025). Their findings indicate that the contact number of droplets can range from 4 to 65, depending on the droplet size distribution's shape and the droplet class's diameter. Additionally, their study identified five regular polyhedral shapes commonly occurring in DPZs: tetrahedron, cube, octahedron, dodecahedron, and icosahedron.

### 3. Modeling

This study aims to develop a modeling approach for droplet deformation into polyhedral shapes that accounts for DPZ polydispersity and characterizes deformation using  $r_f$ ,  $r_a$ , and the volume ratio  $\varepsilon_i$  between the droplet's volume and the volume of its corresponding polyhedral shape. This approach enables the straightforward integration of the new deformation model into the droplet coalescence model proposed by Henschke (1995, 2002). The modeling approach is derived in a generalized form applicable to all regular polyhedral shapes, building upon the foundational principles of Henschke's deformation model (Henschke, 1995).

Furthermore, generalized semi-empirical correlations based on the  $Bo$  number are proposed to describe droplet deformation into regular and irregular convex polyhedral shapes with a uniform edge length  $a$ . It is assumed that the deformation behavior of droplets into regular and irregular convex polyhedral shapes with a uniform edge length  $a$  is comparable. Consequently, the insights gained from modeling droplet deformation into regular polyhedral shapes can be applied to the deformation of droplets into these irregular convex shapes.

In addition, it is assumed that the density difference  $\Delta\rho$  between the two liquid phases, the interfacial tension  $\sigma$ , the average volume fraction  $\varepsilon_p$  of the dispersed phase in the DPZ and the height  $h$  of the DPZ acting on the droplet are known material system and operating parameters, or are obtained from established models (Henschke, 1995, 2002; Leleu and Pfennig, 2019).

The typical geometric relationships for polyhedra, polygons, and spheres used in this study are documented in Bronshtein (2007). The deduced geometric and volumetric relationships are generalized for regular polyhedral shapes by incorporating polyhedral shape-dependent constants  $C_p$ , which are listed in the supporting information (SI) Tab. 1 and include  $C_A$ ,  $C_{re}$ ,  $C_{rm}$ ,  $C_V$ , and  $C_{rs}$ .

According to the droplet deformation model proposed by Henschke (1995, 2002), the degree of deformation of a droplet  $i$  is characterized by the radii  $r_f$  and  $r_a$  as well as the edge length  $a$ . Since  $r_f$ ,  $r_a$ , and  $a$  are unknown, a system of three equations is required to establish the connection between these parameters and the deformation conditions. The pressure relationship, geometric relationship, and volumetric relationship define these equations.

#### 3.1. Pressure relationship

Fig. 1 illustrates the relevant parameters involved in droplet deformation, exemplified for two equal-sized droplets deformed into a cubic shape. Additionally, the contact area  $A_f$  between the droplets is highlighted in yellow, while the curvature regions are highlighted in violet.

Each droplet  $i$  within the DPZ experiences a pressure  $p$ , generated by the buoyancy force exerted by the DPZ droplets affecting droplet  $i$ . This pressure drives the deformation of the droplets and is defined by Eq. (1), where  $g$  is the gravitational constant.

$$p = \Delta\rho g \varepsilon_p h \quad (1)$$

Since the droplets deform from a spherical shape into a polyhedral shape,  $p$  acts on each polyhedral face area  $A_p$ . The area  $A_p$  is dependent on the specific polyhedral shape and is generally determined by Eq. (2).

$$A_p = C_A a^2 \quad (2)$$

According to Henschke, the contact area  $A_f$  does not form a perfect circle but rather a polygonal shape corresponding to the polyhedron's face, with rounded corners (Henschke, 1995). However, Henschke's coalescence model employs the radius  $r_f$ , which is derived from  $A_f$  using Eq. (3). Here,  $r_f$  represents the radius of a circle with an area equal to  $A_f$ , approximating the polygon.

$$A_f = \pi r_f^2 \quad (3)$$

The pressure  $p_f$  acting on the contact area  $A_f$  is related to the pressure  $p$  and the area  $A_p$  according to Eq. (4) (Henschke, 1995).

$$p_f A_f = p A_p \quad (4)$$

The pressure  $p_f = p_{in} - p_{out}$  arises from the pressure difference between the pressure inside the droplet  $p_{in} = p_h + p + p_d$  and the pressure outside the droplet  $p_{out} = p_h + p + p_s$ . Here,  $p_h$  is the hydrostatic pressure,  $p_d$  is the excess pressure inside the droplet relative to its bulk phase, as described by the Young-Laplace equation (de Gennes et al., 2004), and  $p_s$  is the excess pressure within the drainage film between the droplets, resulting from the droplets being pushed together.

The pressure difference between  $p_{in}$  and  $p_{out}$  drives the formation of curvature regions with the radius  $r_a$ . Thus,  $r_a$  is related to this pressure difference by the Young-Laplace equation, as shown in Eq. (5) (Henschke, 1995).

$$p_f = p_{in} - p_{out} = \frac{2\sigma}{r_a} \quad (5)$$

Moreover, the pressure outside the droplet,  $p_{out}$ , depends on the location considered. Behind the rim of the droplet,  $p_s = 0$ , and  $p_{out}$  reaches its minimum value,  $p_{out} = p_{out,r}$ , which is equal to  $p_{out,r} = p_h + p$ . In the center of the film,  $p_{out}$  reaches its maximum value,  $p_{out} = p_{out,c}$ . The increase in pressure from the rim to the center is approximated according to Eq. (6) (Chen et al., 1984).

$$p_{out,c} = p_{out,r} + \frac{\sigma}{r_a} = p_h + p + \frac{\sigma}{r_a} \quad (6)$$

Further, Eq. (5) is considered at two boundary deformation stages. When the DPZ height affecting the droplet is approaching zero, no deformation occurs ( $p \rightarrow 0$ ,  $p_s \rightarrow 0$ ) and  $p_{out}$  becomes independent of the considered location reaching its minimum value, which is equal to  $p_h$  in this case (Abid and Chesters, 1994). At this deformation stage, the radius of the droplet's curvature regions approaches the droplet's radius with  $r_a \rightarrow r$  (Henschke, 1995), and Eq. (5) results in Eq. (7).

$$p_{f,min} = p_d = \frac{2\sigma}{r_a} \quad (7)$$

When  $p \rightarrow \infty$ , maximum deformation is reaching and  $p_{out}$  approaches its maximum value of  $p_{out} \rightarrow p_{out,c}$  according to Eq. (6). At this deformation stage, the droplet's volume becomes almost equivalent to the polyhedron volume with  $r_a \rightarrow 0$  (Henschke, 1995), and Eq. (5) results in Eq. (8).

$$p_{f,max} = p_d - \frac{\sigma}{r_a} = \frac{\sigma}{r_a} \quad (8)$$

To describe the pressure  $p_f$  at all deformation stages from  $p \rightarrow 0$  to  $p \rightarrow \infty$ , Henschke proposed Eq. (9).

$$\bar{p}_f = \frac{2\sigma}{r_a \left(2 - \frac{r_a}{r}\right)} \quad (9)$$

Combining the introduced equations, the pressure relationship is represented by Eq. (10). Since  $\Delta\rho$ ,  $\bar{\varepsilon}_p$ , and  $h$  are assumed to be known parameters,  $p$  is a known parameter (Eq. (1)). The resulting pressure relationship is similar to the one proposed by Henschke (1995) but is derived from the participating pressures more precisely in this work.

$$\pi r_f^2 \frac{2\sigma}{r_a \left(2 - \frac{r_a}{r}\right)} = C_A a^2 p \quad (10)$$

### 3.2. Geometric relationship

Although  $r_f$ ,  $r_a$ , and  $a$  are dependent on the specific polyhedral shape, a general geometric relationship connects them through the intersection area  $A_s$  and the polyhedron face area  $A_p$ . Fig. 2 illustrates this geometric relationship, exemplified by the tetrahedron shape, and is used to derive the general relationship. In Fig. 2a, the intersection area  $A_s$  (in blue) is perpendicular to the polyhedron edge  $b$  and intersects the point  $P$  located at the center of  $b$ . Thus,  $A_s$  passes through the center of the

polyhedron corresponding to the contact areas  $A_f$  (in yellow) located at the face areas  $A_p$ . The shapes of  $A_s$  and  $A_p$  depend on the polyhedron's shape. However, the location of  $A_s$  is defined by the polyhedron edge  $b$  and point  $P$  shape-independent. In Fig. 2b and c, the areas  $A_p$  and  $A_s$  are illustrated, respectively. Additionally, all relevant polyhedral shape parameters involved in droplet deformation and the shape of the deformed droplet (in green) are shown.

The area  $A_f$  is approximated by a polygon with angular corners (Fig. 2b) according to Eq. (11), where  $y$  is the polygon edge length.

$$A_f = C_A y^2 \quad (11)$$

The edge length  $y$  is related to the incircle radius  $r_o$  of this polygon according to Eq. (12).

$$y = \frac{r_o}{C_{rc}} \quad (12)$$

The relationship in Eqs. (11) and (12) matches the boundary condition at  $p \rightarrow \infty$ , since at this condition  $r_o \rightarrow r_c$ ,  $y \rightarrow a$ , and thus,  $A_f \rightarrow A_p$ , with  $r_c$  as the incircle radius of the polygon representing the polyhedron's face  $A_p$ . Moreover, the boundary condition at  $p \rightarrow 0$  is matched, since at this condition  $r_o \rightarrow 0$ ,  $y \rightarrow 0$ , and thus,  $A_f \rightarrow 0$ .

Furthermore, the radius  $r_o$  and the parameters  $r_a$  and  $a$  are geometrically connected through the incircle radius  $r_c$ . The radius  $r_c$  is determined according to Eq. (13).

$$r_c = C_{rc} a \quad (13)$$

In addition,  $r_c$  is determined by the degree of deformation and thus connected to the radius  $r_o$  according to Eq. (14), where  $x$  is the distance between point  $P$  and the polygon border of the contact area  $A_f$ .

$$r_c = r_o + x \quad (14)$$

The distance  $x$  is determined according to Eq. (15), where  $\alpha$  is half the angle between two polyhedron faces.

$$x = \frac{r_a}{\tan(\alpha)} \quad (15)$$

According to Eq. (16), the angle  $\alpha$  is expressed by the radius  $r_c$  (Eq. (13)) and the polyhedron's midsphere radius  $r_m = C_{rm} a$ .

$$\alpha = \arccos\left(\frac{r_c}{r_m}\right) = \arccos\left(\frac{C_{rc}}{C_{rm}}\right) \quad (16)$$

Combining the introduced equations the general geometric relationship is represented by Eq. (17). Compared to the geometric relationship proposed by Henschke (1995), the presented relationship is explicit and requires no correction factors.

$$\left(\frac{\pi C_{rc}^2}{C_A}\right)^{1/2} r_f + \frac{r_a}{\tan\left(\arccos\left(\frac{C_{rc}}{C_{rm}}\right)\right)} = C_{rc} a \quad (17)$$

### 3.3. Volumetric relationship

Although the volume of the deformed droplet depends on the polyhedral shape, it is described by a general volumetric relationship. Fig. 2 illustrates this volumetric relationship, exemplified by the tetrahedron shape, and is used to deduce the general relationship. As proposed by Henschke (1995), the volume of the deformed droplet is approximated by subtracting the channel volume  $V_c$  (in orange) of the curvature region from the polyhedron volume  $V_p$ . Moreover, due to the conservation of mass, the resulting volume of the deformed droplet is equal to the volume  $V$  of the undeformed droplet, as given by Eq. (18), where  $N_e$  is the number of polyhedron edges according to SI Tab. 1.

$$V = V_p - N_e V_c \quad (18)$$

The volume of the undeformed droplet is given by  $V = \frac{\pi}{6} d^3$ , with  $d = 2r$  as the equivalent droplet diameter. The polyhedron volume is determined according to Eq. (19).

$$V_p = C_V a^3 \quad (19)$$

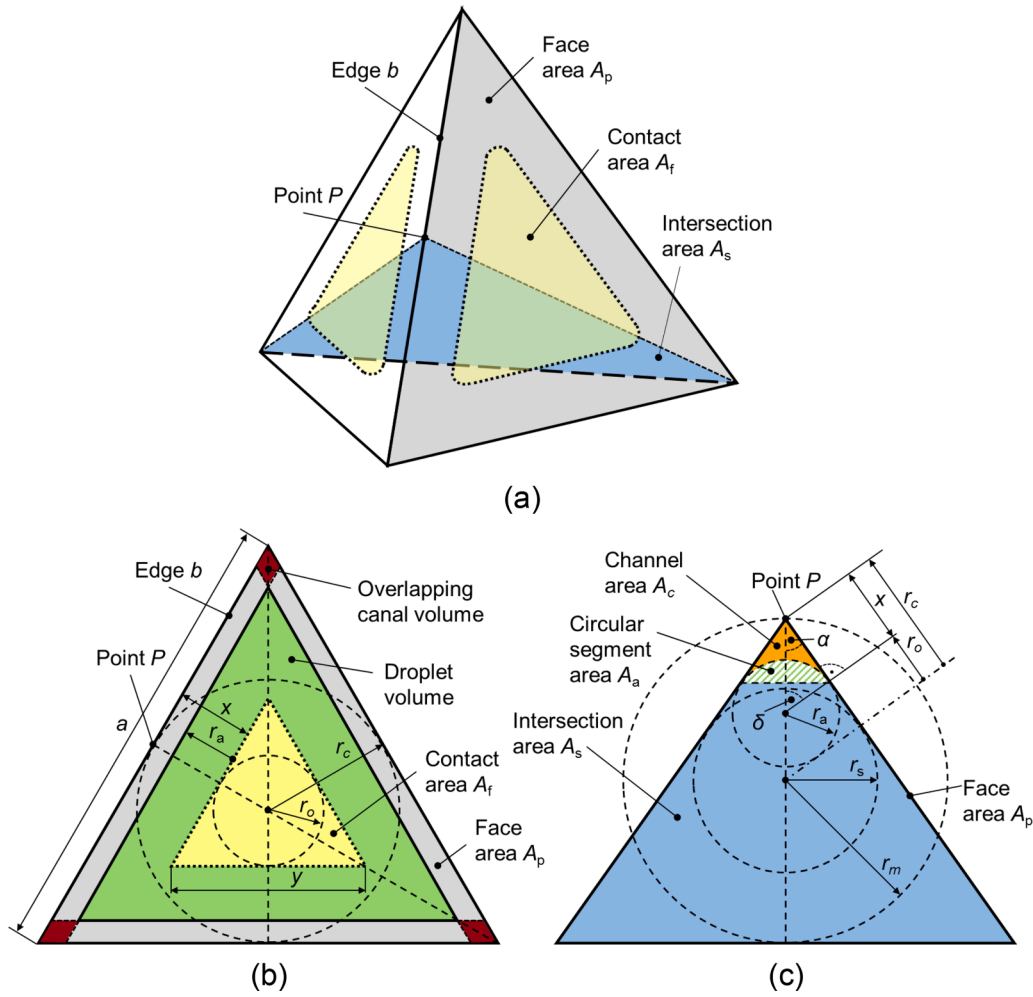


Fig. 2. Geometric relationship between the contact area radius  $r_f$ , the curvature radius  $r_a$  and the polyhedron edge length  $a$ , exemplified by the tetrahedron shape.

The channel volume is approximated according to Eq. (20), where  $A_c$  is the channel area and  $C_{cor}$  is a correction factor.

$$V_c = C_{cor} a A_c \quad (20)$$

The channel area  $A_c = A_t - A_a$  (orange area in Fig. 2c) is the difference between the area  $A_t$  of an isosceles triangle with side length  $x$  and angle  $2\alpha$ , and the area  $A_a$  of the circular segment (hashed green area in Fig. 2c). The areas  $A_t$  and  $A_a$  are determined by Eqs. (21) and (22), respectively, where  $\delta$  is located in the same right-angled triangle as  $\alpha$  and is determined by  $\delta = \pi/2 - \alpha$ . In Eq. (22),  $\delta$  is inserted in radian.

$$A_t = \frac{x^2 \sin(2\alpha)}{2} = \left( \frac{r_a}{\tan(\alpha)} \right)^2 \frac{\sin(2\alpha)}{2} \quad (21)$$

$$A_a = \frac{r_a^2 (2\delta - \sin(2\delta))}{2} \quad (22)$$

The correction factor  $C_{cor}$  is required because the channels overlap (red area in Fig. 2b), leading to an overestimation of the channel volume by Eq. (20) in the absence of this factor. To determine the correction factor, Eqs. (18)–(21) are considered at the boundary condition  $p \rightarrow 0$ . At this deformation state, the radius  $r$  of the undeformed droplet approaches the radius  $r_s = C_{rs} a$  of the polyhedron's insphere, and  $r_a \rightarrow r = r_s$ . Therefore, the correction factor  $C_{cor}$  is derived according to Eq. (23) with  $\alpha$  given by Eq. (16).

$$C_{cor} = \frac{2 \left( C_V - \frac{4\pi}{3} C_{rs}^3 \right)}{N_e C_{rs}^2 \left( \frac{\sin(2\alpha)}{\tan^2(\alpha)} - (\pi - 2\alpha - \sin(2\alpha)) \right)} \quad (23)$$

Combining the introduced equations the general volumetric relationship is represented by Eq. (24). The resulting volumetric relationship is similar to the relationship proposed by Henschke (1995). However, the channel area is derived more precisely and the required relationships are derived in a general form in this work.

$$\frac{\pi}{6} a^3 = C_V a^3 - \frac{C_{cor} N_e}{2} \left( \frac{\sin(2\alpha)}{\tan^2(\alpha)} - (\pi - 2\alpha - \sin(2\alpha)) \right) a r_a^2 \quad (24)$$

### 3.4. Boundary conditions and initial values

Before solving the equation system, boundary conditions for the parameters  $r_f$ ,  $r_a$ , and  $a$  are defined. If a boundary condition equals zero,  $10^{-9}$  is used instead of 0 to avoid numerical issues.

When the pressure  $p \rightarrow 0$ , the radii  $r_f$  and  $r_a$  approach their boundary conditions:  $r_{f,min} = 0$  and  $r_{a,max} = r$ . Moreover, the radius of the undeformed droplet is equal to the radius  $r_s$  of the polyhedron's insphere at this state ( $r = r_s = C_{rs} a$ ), resulting in  $a_{max} = r/C_{rs}$ .

When the pressure  $p \rightarrow \infty$ , the radius  $r_a$  approaches its boundary conditions:  $r_{a,min} = 0$ . In addition, at this pressure the area  $A_f \rightarrow A_p$  resulting in  $r_{f,max} = a_{min} \left( \frac{C_A}{\pi} \right)^{1/2}$  (Eq. (3) and Eq. (2)). Moreover, the polyhedron volume  $V_p = C_V a^3$  is equal to the droplets volume  $V = \frac{4\pi}{3} r$  at this condition, resulting in  $a_{min} = \left( \frac{4\pi}{3C_V} \right)^{1/3} r$ .

Based on these considerations the boundary conditions for  $r_f$ ,  $r_a$ , and  $a$  are defined according to Eqs. (25), (26), and (27), respectively.

$$10^{-9} \leq r_f \leq \left( \frac{C_A}{\pi} \right)^{1/2} \left( \frac{4\pi}{3C_V} \right)^{1/3} r \quad (25)$$



$$10^{-9} \leq r_a \leq r \quad (26)$$

$$\left(\frac{4\pi}{3C_V}\right)^{1/3} r \leq a \leq \frac{r}{C_{rs}} \quad (27)$$

The initial guess values are defined according to Eqs. (28)–(30) with minimum and maximum values from the boundary conditions according to Eqs. (25)–(27).

$$a_0 = a_{\min} + (a_{\max} - a_{\min})/2 \quad (28)$$

$$r_{a,0} = (r_{a,\max} - r_{a,\min})/2 \quad (29)$$

$$r_{f,0} = C_{rc} a_0/2 \quad (30)$$

### 3.5. Volume ratio

The volume ratio between the droplet's original volume and the volume of its corresponding polyhedral shape is determined according to Eq. (31).

$$\varepsilon_i = \frac{V}{V_p} = \frac{\pi}{6C_V} \left(\frac{d}{a}\right)^3 \quad (31)$$

Considering the boundary conditions introduced in Ch. 3.4,  $a \rightarrow a_{\max} = r/C_{rs}$ , when the pressure  $p \rightarrow 0$ , resulting in  $\varepsilon_i \rightarrow \varepsilon_{i,\min}$  according to Eq. (32). When the pressure  $p \rightarrow \infty$ ,  $\varepsilon_i \rightarrow \varepsilon_{i,\max} = 1$ .

$$\varepsilon_{i,\min} = \frac{4\pi C_{rs}^3}{3C_V} \quad (32)$$

### 3.6. Model application to polydisperse systems

The presented modeling approach is derived for a single droplet  $i$  with radius  $r$ . Therefore,  $r_f$  and  $r_a$ , as described in Ch. 3.1–3.4, represent the deformation characteristic radii for this single droplet or a monodisperse droplet size distribution. However, to calculate the coalescence between two droplets in a polydisperse droplet size distribution using Henschke's coalescence model (Henschke, 1995, 2002),  $r_f$  and  $r_a$  cannot be determined based on  $r$ . Coalescence is a binary phenomenon that occurs between a droplet pair, and the droplet radii can differ in polydisperse droplet size distributions. Therefore, instead of  $r$ , an equivalent droplet radius  $r_{eq}$ , as given by Eq. (33) (Abid and Chesters, 1994), is used to calculate  $r_f$  and  $r_a$  using the approach presented in this work (Ch. 3.1–3.4). In Eq. (33),  $r_1$  and  $r_2$  represent the radii of droplet one and droplet two, respectively.

$$r_{eq} = \frac{2}{\frac{1}{r_1} + \frac{1}{r_2}} \quad (33)$$

Moreover, instead of  $h$  and  $p$ ,  $h_{eq}$  and  $p_{eq}$  are used as equivalent DPZ height and pressure acting on the droplet pair. Therefore,  $h_{eq}$  and  $p_{eq}$  are considered in the center between two droplets instead of at the droplet's center.

In contrast,  $\varepsilon_i$  is determined for each individual droplet. To explicitly distinguish between a droplet pair and an individual droplet in this study,  $r_i$ ,  $h_i$ , and  $p_i$  are used instead of  $r$ ,  $h$ , and  $p$  when referring to an individual droplet.

### 3.7. Bond number correlation

The iterative solution of the equation system is a time-consuming task, especially when used to simulate the droplet deformation in a DPZ of thousands of droplets over a long period. Therefore, the  $Bo$  number correlations proposed by Henschke (1995) are used as a quick calculation approach.

The  $Bo$  number is defined by Eq. (34) and the pressure  $p$  is calculated according to Eq. (1) with  $p = p_{eq}$  and  $d = d_{eq}$  used for determining  $r_f$  and  $r_a$  and  $p = p_i$  and  $d = d_i$  used for determining  $\varepsilon_i$ .

$$Bo = \frac{pd}{\sigma} \quad (34)$$

In contrast to the  $Bo$  number expression proposed by Henschke (1995), the pressure in Eq. (34) considers  $\bar{\varepsilon}_p$  (Eq. (1)). This consideration is reasonable because only the dispersed phase within the DPZ is responsible for the deformation of the droplets and not the bulk phase (Ch. 3.1). The bulk phase only participates in the hydrostatic pressure  $p_h$ . Moreover, since the equation system (Ch. 3.1–3.3) considers the pressure according to Eq. (1), it is logical to include the same pressure for the correlation of  $r_f$ ,  $r_a$ , and  $\varepsilon_i$  by the  $Bo$  number. Furthermore, Henschke reported an overestimation due to the  $Bo$  number correlation defined in his work (Henschke, 1995). Since the pressure according to Eq. (1) is lower than the pressure defined by Henschke (1995), the issue of overestimation is also faced by the pressure definition in this work.

Eqs. (35) and (36) (Henschke, 1995) represent the general form of the  $Bo$  number correlations for  $r_f$  and  $r_a$ , respectively, with  $d_{eq} = 2r_{eq}$  as equivalent droplet diameter and  $C_j$  as fitting parameters determined for each polyhedral shape individually.

$$\frac{2r_f}{d_{eq}} = C_1 \sqrt{1 - \frac{C_2}{Bo + C_2}} \quad (35)$$

$$\frac{2r_a}{d_{eq}} = 1 - \sqrt{1 - \frac{C_3}{Bo + C_3}} \quad (36)$$

The fitting parameter  $C_1$  can be determined by considering the boundary conditions (Ch. 3.4) at  $p_{eq} \rightarrow \infty$ , where  $Bo \rightarrow \infty$  and  $r_f \rightarrow \left(\frac{C_A}{\pi}\right)^{1/2} \left(\frac{4\pi}{3C_V}\right)^{1/3} r_{eq}$  (Eq. (25)), resulting in  $C_1 = \left(\frac{C_A}{\pi}\right)^{1/2} \left(\frac{4\pi}{3C_V}\right)^{1/3}$  and Eq. (37). The remaining fitting parameters are fitted to the results of the iterative solution of the equation system.

$$\frac{2r_f}{d_{eq}} = \left(\frac{C_A}{\pi}\right)^{1/2} \left(\frac{4\pi}{3C_V}\right)^{1/3} \sqrt{1 - \frac{C_2}{Bo + C_2}} \quad (37)$$

The  $Bo$  number correlation for  $\varepsilon_i$  is determined based on the results of the iterative solution. Moreover, generalized  $Bo$  number correlations with fitting parameters independent of the polyhedral shape are determined. Assuming the relationship between  $r_a$ ,  $r_f$ ,  $\varepsilon_i$ , and the  $Bo$  number holds for both regular and irregular convex polyhedral shapes with uniform  $a$  (Ch. 3), these correlations can approximate  $r_a$ ,  $r_f$ , and  $\varepsilon_i$  for irregular convex polyhedral shapes.

Since all influencing parameters besides the polyhedral shape parameters are included in the  $Bo$  number, no dimensional analysis is performed to identify the suitable parameters for the generalization of the  $Bo$  number correlations. Instead, the values of the fitting parameters are compared to the polyhedral shape parameters (SI Tab. 1) and appropriate polyhedral shape parameters for the generalization are identified based on their similarities.

In addition, only the following polyhedral shape parameters (SI Tab. 1) are considered for the generalization, as these are unambiguously defined: number of polyhedron faces  $N_f$ , number of polyhedron edges  $N_e$ , number of polyhedron corners  $N_c$  and number of polyhedron's face corners  $N_{fc}$ . Irregular convex polyhedral shapes with uniform  $a$  consist of different face shapes. Thus, polyhedral shape parameters such as  $A_p$  or  $r_o$  are not considered for the generalization, as these are not unique for some polyhedral shapes. The generalized  $Bo$  number correlations are fitted to all iterative solution results.

### 3.8. Parameter range

The deformation described by the presented model is dependent on the parameters  $d$ ,  $\sigma$  and  $p$ , which is further determined by  $\Delta\rho$ ,  $\bar{\varepsilon}_p$ , and  $h$ . The value ranges of these parameters are set to match the technical applications to investigate the model performance in a relevant range. The following ranges are identified:  $d = 150$ – $1500 \mu\text{m}$  (Sibirtsev et al., 2024, 2025),  $\sigma = 2$ – $50 \text{ mN/m}$  (Henschke, 1995),  $\Delta\rho = 30$ – $350 \text{ kg/m}^3$  (Henschke, 1995),  $\bar{\varepsilon}_p = 0.55$ – $1.0$  (Henschke, 1995; Sibirtsev et al., 2025),  $h = 1$ – $50 \text{ mm}$  (Henschke, 1995), resulting in  $p \approx 0.2$ – $200 \text{ Pa}$ .

The  $Bo$  number range results in  $Bo \approx 0$ –150 based on these parameter ranges. In technical applications at industrial scale, higher  $d$  and  $h$  can occur, resulting in even higher  $Bo$  values. However, it is unnecessary to consider these high values when investigating the model since Henschke (1995) showed that at  $Bo \approx 50$ , the droplet deformation almost reaches its final deformation stage. At this stage,  $r_a$  and  $r_f$  reach their limit values, which are  $r_a \rightarrow 0$  and  $r_f \rightarrow r_{f,max}$ . Increasing the  $Bo$  number further does not significantly affect  $r_a$  and  $r_f$  from this deformation stage onwards.

### 3.9. Iterative solution of the equation system and fitting procedure

With Eqs. (10), (17) and (24), the unknown parameters  $r_f$ ,  $r_a$  and  $a$ , the set parameters  $d$ ,  $\sigma$ , and  $p$ , as well as the polyhedral shape-dependent constants  $C_p$  (SI Tab. 1), the equation system is fully defined. A publicly accessible Python code (Sibirtsev, 2025) is used to solve the equation and to fit the  $Bo$  correlation parameters. The equation system is solved within the specified  $d$ ,  $\sigma$ , and  $p$  ranges (Ch. 3.8). Each range is divided into ten steps. Thus, the equation system is solved at 1000 points for each polyhedral shape, resulting in 5000 simulations. For the solution of the equations system, the `scipy.optimize.minimize()` method (Virtanen et al., 2020) is used. Moreover, the Nelder-Mead solver (Virtanen et al., 2020) is used at  $Bo \leq 1$  and the Powell solver (Virtanen et al., 2020) at  $Bo > 1$ , since it delivers the most accurate results in this work. The mean absolute percentage error (MAPE) according to Eq. (38) is used as minimization function, where  $E_{L,j}$  and  $E_{R,j}$  are the results of the left and the right hand side of the  $N_E = 3$  equations, Eqs. (10), (17), and (24). Solutions with a MAPE<sub>1</sub> value higher than 1 % are excluded from further consideration.

$$MAPE_1 = 100 \frac{1}{N_E} \sum_{j=1}^{N_E} \left| \frac{E_{L,j} - E_{R,j}}{E_{L,j}} \right| \quad (38)$$

The results of the iterative solution of  $r_f$ ,  $r_a$  and  $\varepsilon$  are not equally distributed over the  $Bo$  number range. Therefore, the  $Bo$  number values are transformed into a logarithmic scale to achieve a more even distribution of the data. Moreover, equally spaced bins within the transformed  $Bo$  number range are defined, and an equal number of randomly chosen iterative solution results within these bins is used to fit the  $Bo$  number correlation parameters. In this manner, a similar accuracy of the  $Bo$  number correlation is given over the entire range of the  $Bo$  number. For the fitting, the *Sequential Least Squares Programming* (SLSQP) solver of the `scipy.optimize.minimize()` method (Virtanen et al., 2020) is used since it is a fast solver and provides accurate results in this case. The MAPE, according to Eq. (39) is used as a minimization function for the fit, where  $N_p$  is the number of fitted points,  $A_j$  are the results of the iterative solution, and  $P_j$  are the predicted values by the  $Bo$  number correlation. In addition, the MAPE<sub>3</sub> is considered to make a statement about how accurate the fit is across all the simulations performed in this work. The MAPE<sub>3</sub> is equally defined as MAPE<sub>2</sub> (Eq. (39)) but takes all the results  $N_r$  of the iterative solution into account instead of  $N_p$ .

$$MAPE_2 = 100 \frac{1}{N_p} \sum_{j=1}^{N_p} \left| \frac{A_j - P_j}{A_j} \right| \quad (39)$$

All simulations are performed on an Intel Core i7-3740QM CPU.

## 4. Results & discussion

From 5000 simulations, approx. 29 % solutions of the equation system result in an MAPE<sub>1</sub> (Eq. (38)) over 1 %, and thus, are excluded from further consideration. The most of the results with MAPE<sub>1</sub> > 1 % are achieved at low  $p$  values. At these conditions, the  $Bo$  number values are low, which means that  $r_f$  is approaching its limit value of zero. One assumption is that it is difficult to achieve convergence in this area due to the strong gradient in the courses of  $r_f$  and  $r_a$ .

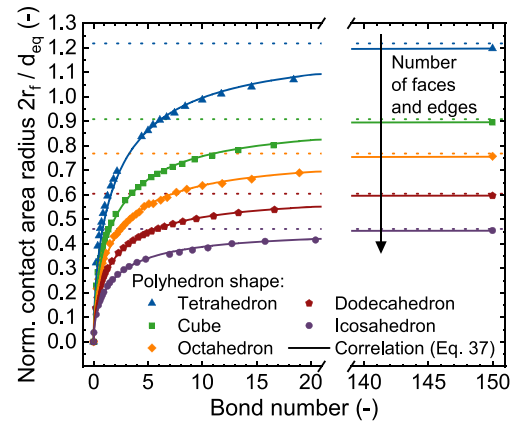


Fig. 3. Dependency of the normalized contact area radius  $2r_f/d_{eq}$  on the  $Bo$  number for iterative solution results (points) and  $Bo$  number correlation (solid lines).

All equation system solutions with MAPE<sub>1</sub> ≤ 1 % are used to investigate the dependency of  $r_f$ ,  $r_a$  and  $\varepsilon_i$  on the  $Bo$  number and to fit the fitting parameters of the Eqs. (37) and (36). The resulting fitting parameters can be found in SI Tab. 2. For clarity, only every 25th point of the simulations is shown in the following graphs.

### 4.1. Contact area radius $r_f$

Fig. 3 shows the normalized contact area radius  $2r_f/d_{eq}$  in dependence on the  $Bo$  number for iterative solution results (points) and  $Bo$  number correlation Eq. (37) (solid lines). The  $2r_f/d_{eq}$  increases with increasing  $Bo$  number. The slope of the curves is steep at the beginning and decreases with an increase in the  $Bo$  number, whereby the course approaches a limit value (dotted lines). The observed change in the slope is because the contact area  $A_f$  is increasing linearly proportional with an increase in  $p_i$  or a decrease in  $\sigma$  (Eqs. (3) and (10)), and thus, an increase in the  $Bo$  number (Eq. (34)). Since  $r_f$  is proportional to the square root of  $A_f$ , the course follows a square root function as also shown by Henschke (1995). The correlation Eq. (37) matches this curve progression accurately with an MAPE<sub>2</sub> of 1.7 % and an MAPE<sub>3</sub> of 2.9 % averaged over the five polyhedral shapes.

Moreover, the limit value of  $2r_f/d_{eq}$  is dependent on the polyhedral shape and decreases with the number of polyhedron faces and edges for a constant  $Bo$  number. Since the area potentially available as the droplet contact area  $A_f$  decreases with the number of faces, and thus, decreasing polyhedron face area  $A_p$ , the limit value of  $2r_f/d_{eq}$  also decreases. For the dodecahedron, a limit value of approx. 0.6 is reached in this work. This value is also reached by the deformation modeling performed by Henschke (1995).

### 4.2. Curvature radius $r_a$

Fig. 4a shows the normalized curvature radius  $2r_a/d_{eq}$  in dependence on the  $Bo$  number for iterative solution results (points) and the  $Bo$  number correlation Eq. (36) (solid lines). The radius  $2r_a/d_{eq}$  decreases with an increasing  $Bo$  number. The slope of the curves is steep at the beginning and decreases with the increase in the  $Bo$  number, whereby the course approaches a limit value of zero. The observed change in the slope is because  $r_a$  is decreasing almost linearly anti-proportional with an increase in  $p_i$  or a decrease in  $\sigma$  (Eq. (10)), and thus, an increase in the  $Bo$  number.

Moreover,  $2r_a/d_{eq}$  is dependent on the polyhedral shape and increases with the number of polyhedron edges for a constant  $Bo$  number. One possible explanation is that the total deformation of a droplet is distributed over all curvature regions of the polyhedron. The more edges a polyhedron has, the higher its number of curvature regions, and

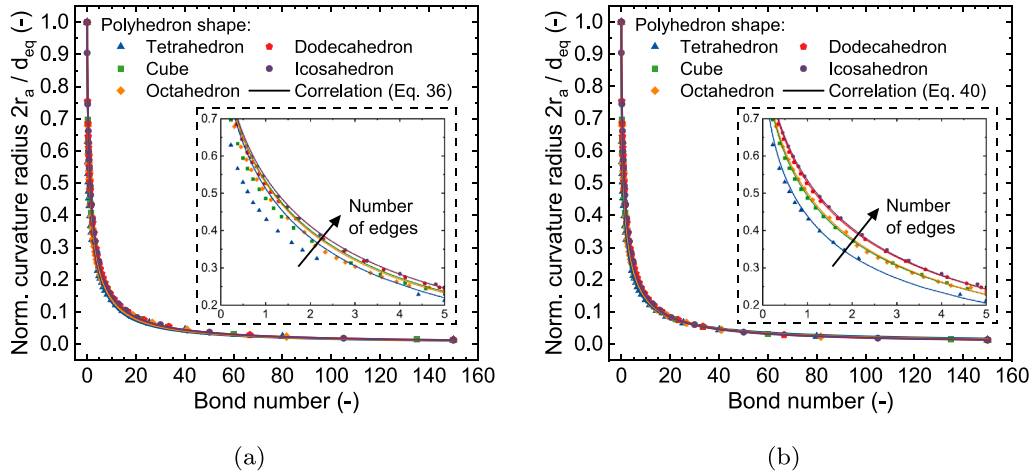


Fig. 4. Dependency of the normalized contact area radius  $2r_a/d_{eq}$  on the  $Bo$  number for iterative solution results (points) and  $Bo$  number correlation (solid lines) according to (a) Eq. (36) and (b) Eq. (40).

the less the deformation in each curvature region, resulting in higher  $r_a$  values. Therefore, at the same  $Bo$  numbers and thus the same degree of deformation, a polyhedral shape with a higher number of edges has a higher  $2r_a/d_{eq}$  value than one with a lower number of edges.

Even though the  $Bo$  number correlation Eq. (36) matches the curve progression with an  $MAPE_2$  of 5.5 % and an  $MAPE_3$  of 5.3 % averaged over the five polyhedral shapes, it overestimates the  $2r_a/d_{eq}$  values in the range of  $Bo = 0.2 \dots 4.5$ . This overestimation is also noticed for the dodecahedron shape by Henschke (1995). It is assumed that one fitting parameter ( $C_3$ ) cannot accurately describe the curve progression by the  $Bo$  number correlation. Therefore, a second fitting parameter is introduced resulting in Eq. (40), with  $C_4$  and  $C_5$  as the fitting parameters. The parameter  $C_5$  is chosen because it allows the adjustment of the slope of the asymptotic curve progression.

$$\frac{2r_a}{d_{eq}} = 1 - \sqrt{1 - \frac{C_4}{Bo^{C_5} + C_4}} \quad (40)$$

Fig. 4b shows the  $2r_a/d_{eq}$  in dependence on the  $Bo$  number according to Eq. (40). The correlation Eq. (40) matches the curve progression in the range of  $Bo = 0.2 \dots 4.5$  more accurately with an  $MAPE_2$  and an  $MAPE_3$  of 2.0 % averaged over the five polyhedral shapes.

#### 4.3. Volume ratio $\varepsilon_i$

Fig. 5 shows the volume ratio  $\varepsilon_i$  in dependence on the  $Bo$  number for iterative solution results (points) and  $Bo$  number correlation (solid lines). The  $\varepsilon_i$  increases with increasing  $Bo$  number, starting at  $\varepsilon_i(Bo = 0) = \varepsilon_{i,min}$  and asymptotically approaching  $\varepsilon_i(Bo \rightarrow \infty) = \varepsilon_{i,max}$  (Ch. 3.5). The slope of the curves is steep at the beginning and decreases with an increase in the  $Bo$  number, whereby the course approaches a limit value of  $\varepsilon_{i,max} = 1$ . The observed change in the slope occurs because the square of the edge length  $a^2$ , increases linearly with an increase in  $p_i$  or a decrease in  $\sigma$  (Eq. (10)), and thus, an increase in the  $Bo$  number (Eq. (34)). As a result,  $a$  follows a square root dependence on  $Bo$ .

Moreover,  $\varepsilon_i$  depends on the polyhedral shape and increases with the number of polyhedron faces and edges for a constant  $Bo$  number. One explanation for this observation is that the polyhedral shape approaches a spherical shape with an increasing number of faces and edges. By approaching the spherical shape, the volume in the channels between the droplets decreases and the volume ratio  $\varepsilon_i$  approaches 1.

The observed curve progression can be described by Eq. (41). The fitting parameter  $C_6$  can be determined by considering the boundary conditions (Ch. 3.4) at  $p_i \rightarrow 0$ , where  $Bo \rightarrow 0$  and  $\varepsilon_i \rightarrow \varepsilon_{i,min} = \frac{4\pi C_{rs}^3}{3C_V}$  (Eq. (32)), resulting in  $C_6 = \frac{4\pi C_{rs}^3}{3C_V}$  and Eq. (42). The fitting parameter

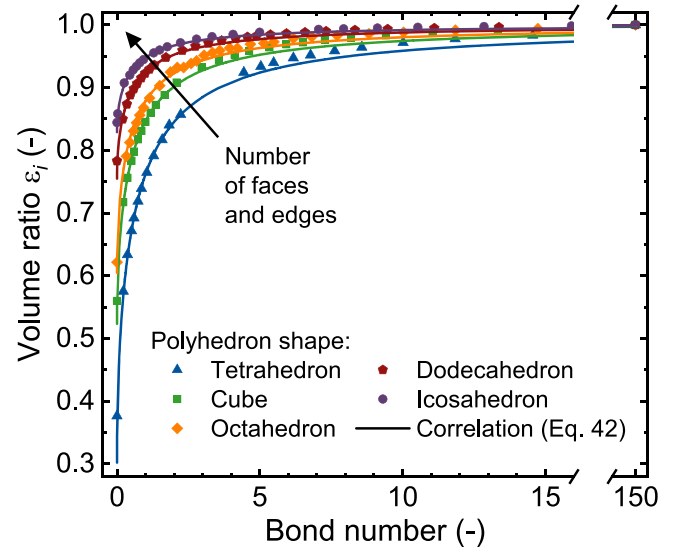


Fig. 5. Dependence of the volume ratio  $\varepsilon_i$  on the  $Bo$  number for iterative solution results (points) and  $Bo$  number correlation (solid line).

$C_7$  is fitted to the results of the iterative solution (SI Tab. 2). The correlation Eq. (42) matches the curve progression accurately with an  $MAPE_2$  and an  $MAPE_3$  of 0.6 % averaged over the five polyhedral shapes. However, at  $Bo > 2$  Eq. (41) slightly underestimates  $\varepsilon_i$ .

$$\varepsilon_i = C_6 + (1 - C_6) \sqrt{1 - \frac{C_7}{Bo + C_7}} \quad (41)$$

$$\varepsilon_i = \frac{4\pi C_{rs}^3}{3C_V} + \left(1 - \frac{4\pi C_{rs}^3}{3C_V}\right) \sqrt{1 - \frac{C_7}{Bo + C_7}} \quad (42)$$

#### 4.4. Generalization of the Bond number correlations

After comparing the polyhedral shape dependent fitting parameters  $C_j$  (SI Tab. 2) with the geometrical parameters of the polyhedral shapes (SI Tab. 1),  $N_f$  and  $N_e$  are chosen to generalize Eqs. (35), (36), and (41) to (43), (44), and (45) with polyhedral shape independent fitting parameters. Since irregular convex polyhedral shapes with uniform  $a$  consist of different face shapes,  $\bar{r}_f$  and  $\bar{r}_a$  are considered as the average contact area radius and the average radius of droplet's curvature regions,



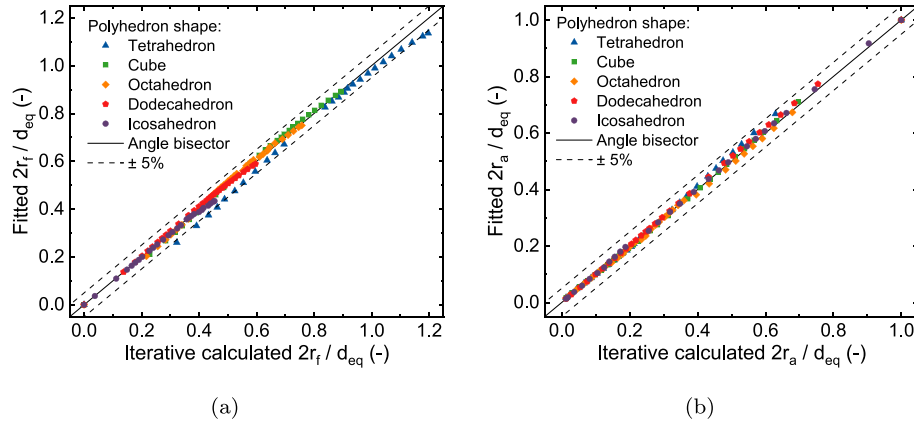


Fig. 6. Comparison between iterative determined (Eqs. (10), (17) and (24)) and fitted (a) (Eq. (43))  $2r_f/d_{eq}$  and (b) (Eq. (44))  $2r_a/d_{eq}$  values.

respectively.

$$\frac{2\bar{r}_f}{d_{eq}} = \frac{2.65}{N_f^{0.6}} \sqrt{1 - \frac{5.0/N_e^{0.1}}{Bo + 5.0/N_e^{0.1}}} \quad (43)$$

$$\frac{2\bar{r}_a}{d_{eq}} = 1 - \sqrt{1 - \frac{1.35N_e^{0.3}}{Bo(0.7N_e^{0.1}) + 1.35N_e^{0.3}}} \quad (44)$$

$$\varepsilon_i = \Psi + (1 - \Psi) \sqrt{1 - \frac{1.41N_e^{0.1}}{Bo + 1.41N_e^{0.1}}} \quad (45)$$

$$\Psi = -8.13 + (1 + 8.13) \sqrt{1 - \frac{0.714}{N_f + 0.714}}$$

The choice of  $N_f$  in Eq. (43) is based on the consistent opposing behavior observed between  $N_f$  and  $C_1$  when the polyhedral shape changes (Fig. 3). The significant influence of  $N_f$  on  $r_f$  is logical, as for the same  $Bo$  numbers and  $d_{eq}$ , polyhedra with a higher number of faces have smaller contact areas  $A_f$  and thus lower  $r_f$  values (Ch. 4.1). In contrast,  $C_2$  correlates most accurately with  $N_e$ . However,  $N_e$  has a smaller influence on  $r_f$  in Eq. (43) compared to  $N_f$ .

The choice of  $N_e$  in Eq. (44) is based on the consistent similar behavior observed between  $N_e$ ,  $C_4$ , and  $C_5$  when the polyhedral shape changes (Fig. 4). The significant influence of  $N_e$  on  $r_a$  is logical, as for the same  $Bo$  numbers and  $d_{eq}$ , a larger curvature radius  $r_a$  is expected for polyhedra with a higher number of edges (Ch. 4.2).

The choice of  $N_e$  and  $N_f$  in Eq. (45) is based on the consistent similar behavior observed between  $N_e$  and  $C_6$ , and the opposing behavior observed between  $N_f$  and  $C_7$  when the polyhedral shape changes (Fig. 5). The influence of  $N_e$  and  $N_f$  on  $\varepsilon_i$  is logical, as for the same  $Bo$  numbers and  $d_i$ , the polyhedral shape approaches a spherical shape with an increasing number of faces, leading to an increase in  $\varepsilon_i$  (Ch. 4.3).

Fig. 6 and SI Fig. 7 show the comparison between iterative determined (Eqs. (10), (17), (24), and (31)) and fitted (Eqs. (43), (44), and Eq. (45))  $2\bar{r}_f/d_{eq}$ ,  $2\bar{r}_a/d_{eq}$ , and  $\bar{\varepsilon}_i$  values. The generalized  $Bo$  number correlations show high accuracies with MAPE<sub>2</sub> of 2.3 %, 2.4 %, and 0.6 % and MAPE<sub>3</sub> of 2.8 %, 2.4 % and 0.6 % for Eqs. (43), (44), and (45), respectively. All  $2\bar{r}_f/d_{eq}$ ,  $2\bar{r}_a/d_{eq}$ , and  $\bar{\varepsilon}_i$  values are located within an interval of  $\pm 5$  %. Only for the tetrahedron shape  $2\bar{r}_f/d_{eq}$  falls below the interval of  $\pm 5$  % at  $2\bar{r}_f/d_{eq} < 0.6$ .

Since Eqs. (43), (44), and (45) incorporate the polyhedral shape parameters,  $N_f$  and  $N_e$ , the presented  $Bo$  number correlations can be utilized not only to predict  $r_f$ ,  $r_a$ ,  $\varepsilon_i$  for regular polyhedral shapes but also to estimate these parameters for irregular convex polyhedral shapes with uniform  $a$ . The specific polyhedral shape adopted by a droplet in the DPZ can be determined using the simulation method outlined by Sibirtsev et al. (2025). This method calculates the contact number of the droplet

within the DPZ, identifying  $N_f$  as the contact number. The parameter  $N_e$  is subsequently determined based on the identified polyhedral shape.

## 5. Conclusion

This study presents a novel modeling approach to characterize droplet deformation into polyhedral shapes within liquid-liquid polydisperse dense-packed zones (DPZs). The deformation is described by two characteristic radii: the contact radius  $r_f$  and the curvature radius  $r_a$ , as well as the volume ratio  $\varepsilon_i$ . These parameters are determined through a system of equations based on pressure, geometric, and volumetric relationships for regular polyhedra. Additionally, generalized correlations based on the Bond ( $Bo$ ) number are introduced to predict droplet deformation for regular polyhedral shapes and to estimate droplet deformation for irregular convex polyhedral shapes. The droplet deformation is simulated across a  $Bo$  number range relevant to technical applications.

The simulation results reveal that the contact radius  $r_f$  increases with increasing  $Bo$  number and decreasing numbers of polyhedron faces and edges, approaching a shape-dependent limit. Conversely, the curvature radius  $r_a$  exhibits the opposite trend, decreasing as  $Bo$  numbers increase and approaching a zero-limit at high  $Bo$  number values. The volume ratio  $\varepsilon_i$  increases with increasing  $Bo$  number and numbers of polyhedron faces and edges, approaching the limit-value of 1. The generalized  $Bo$  number correlations strongly agree with the equation system solutions, achieving mean absolute percentage errors below 3.0 % and an average deviation of less than  $\pm 5$  %.

The findings on droplet deformation into polyhedral shapes provide valuable practical implications. These insights can be applied to predict droplet deformation in liquid-liquid polydisperse DPZs, enhancing the utility and relevance of this research. Furthermore, the proposed modeling approach facilitates seamless integration into Henschke's coalescence model (Henschke, 1995, 2002), as this model uses the same characteristic radii  $r_f$  and  $r_a$ .

In future work, the deformation model will be implemented in a simulation environment to simulate the formation and dissolution of DPZs during the phase separation of polydisperse liquid-liquid dispersions. Furthermore, the validity of the proposed  $Bo$  number correlations for irregular convex polyhedral shapes will be verified by adapting and solving the introduced equation system for such geometries. In addition, the presented modeling approach will be validated by experimental investigations.

## Data availability

The link to the Python source code of this work can be found on GitLab (Sibirtsev, 2025).

## Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

## CRediT authorship contribution statement

**Stepan Sibirtsev:** Writing – original draft, Visualization, Software, Project administration, Methodology, Investigation, Data curation, Conceptualization; **Lukas Thiel:** Writing – review & editing; **Yannik Daner:** Writing – review & editing, Methodology, Investigation; **Andrey Kirsanov:** Writing – review & editing, Methodology, Investigation; **Andreas Jupke:** Writing – review & editing, Supervision, Resources

## Supplementary material

Supplementary material associated with this article can be found in the online version at [10.1016/j.ces.2025.121575](https://doi.org/10.1016/j.ces.2025.121575)

## References

- Abe, K., Inasawa, S., 2022. Deformation and coalescence of particle-stabilized oil droplets in drying aqueous NaCl solutions. *Colloids Surf. A* 632, 127816. <https://doi.org/10.1016/j.colsurfa.2021.127816>
- Abid, S., Chesters, A.K., 1994. The drainage and rupture of partially-mobile films between colliding drops at constant approach velocity. *Int. J. Multiphase Flow* 20 (3), 613–629. [https://doi.org/10.1016/0301-9322\(94\)90033-7](https://doi.org/10.1016/0301-9322(94)90033-7)
- Bozzano, G., Dente, M., 2010. Mechanism of drop coalescence at the interface of two immiscible liquids. In: 20th European Symposium on Computer Aided Process Engineering. Elsevier. Vol. 28 of *Computer Aided Chemical Engineering*, pp. 55–60. [https://doi.org/10.1016/S1570-7946\(10\)28010-0](https://doi.org/10.1016/S1570-7946(10)28010-0)
- Bronstein, I.N., 2007. *Handbook of Mathematics*. Springer, Berlin and New York. 5th ed. edition.
- Chan, D. Y.C., Klaseboer, E., Manica, R., 2011. Film drainage and coalescence between deformable drops and bubbles. *Soft Matter* 7 (6), 2235–2264. <https://doi.org/10.1039/C0SM00812E>
- Chen, J.-D., Hahn, P.S., Slattery, J.C., 1984. Coalescence time for a small drop or bubble at a fluid–fluid interface. *AIChE J.* 30 (4), 622–630. <https://doi.org/10.1002/aic.690300413>
- de Gennes, P.-G., Brochard-Wyart, F., Quéré, D., 2004. *Capillarity and wetting phenomena: Drops, bubbles, pearls, waves*. Springer, New York.
- Dunne, F.F., Winkelman, J., Weaire, D., Hutzler, S., 2019. Implementation of Morse–Witten theory for a polydisperse wet 2D foam simulation. *Philos. Mag.* 99 (18), 2303–2320. <https://doi.org/10.1080/14786435.2019.1624852>
- Eberz, J., Sibirtsev, S., Jupke, A., 2025. Mini-batch settling cell for investigation of liquid–liquid phase separation. *Chem. Eng. Sci.* 301, 120751. <https://doi.org/10.1016/j.ces.2024.120751>
- Eggert, A., Kögl, T., Arlt, W., Jupke, A., 2019. Computer tomographic detection of the liquid–liquid mixing and separation within the annular centrifugal contactor/extractor. *Chem. Eng. Res. Des.* 142, 143–153. <https://doi.org/10.1016/j.cherd.2018.11.034>
- Frising, T., Noik, C., Dalmazzone, C., 2006. The liquid/liquid sedimentation process: from droplet coalescence to technologically enhanced water/oil emulsion gravity separators: a review. *J. Dispers. Sci. Technol.* 27 (7), 1035–1057. <https://doi.org/10.1080/01932690600767098>
- Graham, E.E., Ooi, K.L., Odell, M.H., 1979. Drop size distributions for non-coalescing liquid–liquid systems in sieve plate columns. *The Chemical Engineering Journal* 18 (3), 189–196. [https://doi.org/10.1016/0300-9467\(79\)80117-3](https://doi.org/10.1016/0300-9467(79)80117-3)
- Henschke, M., 1995. Dimensionierung liegender Flüssig–flüssig-Abscheider anhand diskontinuierlicher Absetzversuche. Vol. Nr. 379 of *Fortschritt-Berichte VDI. Reihe 3, Verfahrenstechnik*. VDI Verlag, Düsseldorf.
- Henschke, M., 2002. Determination of a coalescence parameter from batch-settling experiments. *Chem. Eng. J.* 85 (2–3), 369–378. [https://doi.org/10.1016/S1385-8947\(01\)00251-0](https://doi.org/10.1016/S1385-8947(01)00251-0)
- Höhler, R., Weaire, D., 2019. Can liquid foams and emulsions be modeled as packings of soft elastic particles? *Adv. Colloid Interface Sci.* 263, 19–37. <https://doi.org/10.1016/j.cis.2018.11.002>
- Lacasse, M.D., Grest, G.S., Levine, D., 1996. Deformation of small compressed droplets. *Phys. Rev. E Stat. Phys. Plasmas Fluids Relat. Interdiscip. Top.* 54 (5), 5436–5446. <https://doi.org/10.1103/PhysRevE.54.5436>
- Leleu, D., Pfennig, A., 2019. Coalescence modeling for design of technical equipment. *Chem. Eng. Technol.* 42 (7), 1404–1413. <https://doi.org/10.1002/ceat.201900037>
- Liu, W., Chen, S., Wu, C.-Y., Li, S., 2019. Unified size-density and size-topology relations in random packings of dry adhesive polydisperse spheres. *Phys. Rev. E* 99 (2-1), 022901. <https://doi.org/10.1103/PhysRevE.99.022901>
- Mohanty, S., Vogelpohl, A., 1997. A simplified hydrodynamic model for a pulsed sieve-plate extraction column. *Chem. Eng. Process.* 36 (5), 385–395. [https://doi.org/10.1016/S0255-2701\(97\)00010-X](https://doi.org/10.1016/S0255-2701(97)00010-X)
- Morse, D.C., Witten, T.A., 1993. Droplet elasticity in weakly compressed emulsions. *Eur. Phys. Lett. (EPL)* 22 (7), 549–555. <https://doi.org/10.1209/0295-5075/22/7/012>
- Raynel, G., Marques, D.S., Al-Thabet, M., 2023. The influence of water droplet packing on crude oil emulsion. *Eur. Phys. J. E Soft Matter* 46 (7), 53. <https://doi.org/10.1140/epje/s10189-023-00311-9>
- Rommel, W., Meon, W., Blass, E., 1992. Hydrodynamic modeling of droplet coalescence at liquid–liquid interfaces. *Sep. Sci. Technol.* 27 (2), 129–159. <https://doi.org/10.1080/01496399208018870>
- Schlieper, L., Chatterjee, M., Henschke, M., Pfennig, A., 2004. Liquid–liquid phase separation in gravity settler with inclined plates. *AIChE J.* 50 (4), 802–811. <https://doi.org/10.1002/aic.10075>
- Sibirtsev, S., 2025. Droplet deformation GitLab repository. <https://git.rwth-aachen.de/avt-fvt/public/droplet-deformation>. Access date: 2025-01-11.
- Sibirtsev, S., Göbel, C.B., Jupke, A., 2019. Automation of a procedure for the experimental investigation of liquid–liquid phase separation. *Chem. Ing. Tech.* 91 (12), 1787–1793. <https://doi.org/10.1002/cite.201900162>
- Sibirtsev, S., Thiel, L., Kirsanov, A., Jupke, A., 2025. Droplet contact numbers and contact probabilities in liquid–liquid dense-packed zones. *AIChE J.* <https://doi.org/10.1002/aic.18723>
- Sibirtsev, S., Thiel, L., Zhai, S., Recke, L., Cai, Y.T., Jupke, A., 2024. Experimental and model-based investigation of the droplet size distribution during the mixing process in a batch-settling cell. *Can. J. Chem. Eng.*. Manuscript under review (revision 1)
- Sovilj, M.N., Nikolovski, B.G., Spasojević, M.D., 2019. Hydrodynamics in spray and packed liquid–liquid extraction columns: a review. *M top Maced. J. Chem. Chem. Eng.* 38 (2), 267. <https://doi.org/10.20450/mjce.2019.1519>
- Steinhoff, J., Charlafti, E., Leleu, D., Reinecke, L., Franken, H., Becker, K., Kalem, M., Sixt, M., Braß, M., Borchardt, D., Bäcker, W., Wegener, M., Maaß, S., Weber, M., Acher, T., Matten, C., Pfennig, A., Kraume, M., Bart, H.-J., 2021. Energie- und ressourceneinsparung durch innovative und CFD-basierte auslegung von flüssig–flüssig–schwerkraftabscheidern. *Chem. Ing. Tech.* 93 (7), 1152–1165. <https://doi.org/10.1002/cite.202000083>
- Steinhoff, J., Gebauer, F., Fölsch, D., Bart, H.-J., 2018. Optimized description of dispersion layers on a vertical separator. *Chem. Ing. Tech.* 90 (7), 979–987. <https://doi.org/10.1002/cite.201700092>
- Thaker, A.H., Buwa, V.V., 2019. Experimental investigations of interfacial and binary coalescence of multilayered drops. *Ind. Eng. Chem. Res.* 58 (18), 7620–7632. <https://doi.org/10.1021/acs.iecr.8b05994>
- Thaker, A.H., Darekar, M., Singh, K.K., Buwa, V.V., 2018. Experimental investigations of liquid–liquid disengagement in a continuous gravity settler. *Chem. Eng. Res. Des.* 139, 174–187. <https://doi.org/10.1016/j.cherd.2018.09.031>
- Virtanen, P., Gommers, R., Oliphant, T.E., Haberland, M., Reddy, T., Cournapeau, D., Burovski, E., Peterson, P., Weckesser, W., Bright, J., van der Walt, S.J., Brett, M., Wilson, J., Millman, K.J., Mayorov, N., Nelson, A. R.J., Jones, E., Kern, R., Larson, E., Carey, C.J., Polat, İ., Feng, Y., Moore, E.W., VanderPlas, J., Laxalde, D., Perktold, J., Cimrman, R., Henriksen, I., Quintero, E.A., Harris, C.R., Archibald, A.M., Ribeiro, A.H., Pedregosa, F., van Mulbregt, P., 2020. Scipy 1.0: fundamental algorithms for scientific computing in python. *Nat. Methods* 17 (3), 261–272. <https://doi.org/10.1038/s41592-019-0686-2>
- Weber, B., Jupke, A., 2020. Compartment–model for the simulation of the separation performance of stirred liquid–liquid–extraction columns. *AIChE J.* 66 (8). <https://doi.org/10.1002/aic.16286>
- Ye, S., Hohl, L., Charlafti, E., Jin, Z., Kraume, M., 2023a. Effect of temperature on mixing and separation of stirred liquid/liquid dispersions over a wide range of dispersed phase fractions. *Chem. Eng. Sci.* 274, 118676. <https://doi.org/10.1016/j.ces.2023.118676>
- Ye, S., Hohl, L., Kraume, M., 2023b. Impact of feeding conditions on continuous liquid–liquid gravity separation, Part I: inlet and outlet drop size, dense-packed zone and separation efficiency. *Chem. Eng. Sci.* 282, 119237. <https://doi.org/10.1016/j.ces.2023.119237>